

Strahlenturbulenz

Possibilities of water flow in a pool

Differences to vertical bottom flow

Practice and advantages

Karl Pfeiffer



Since 1988

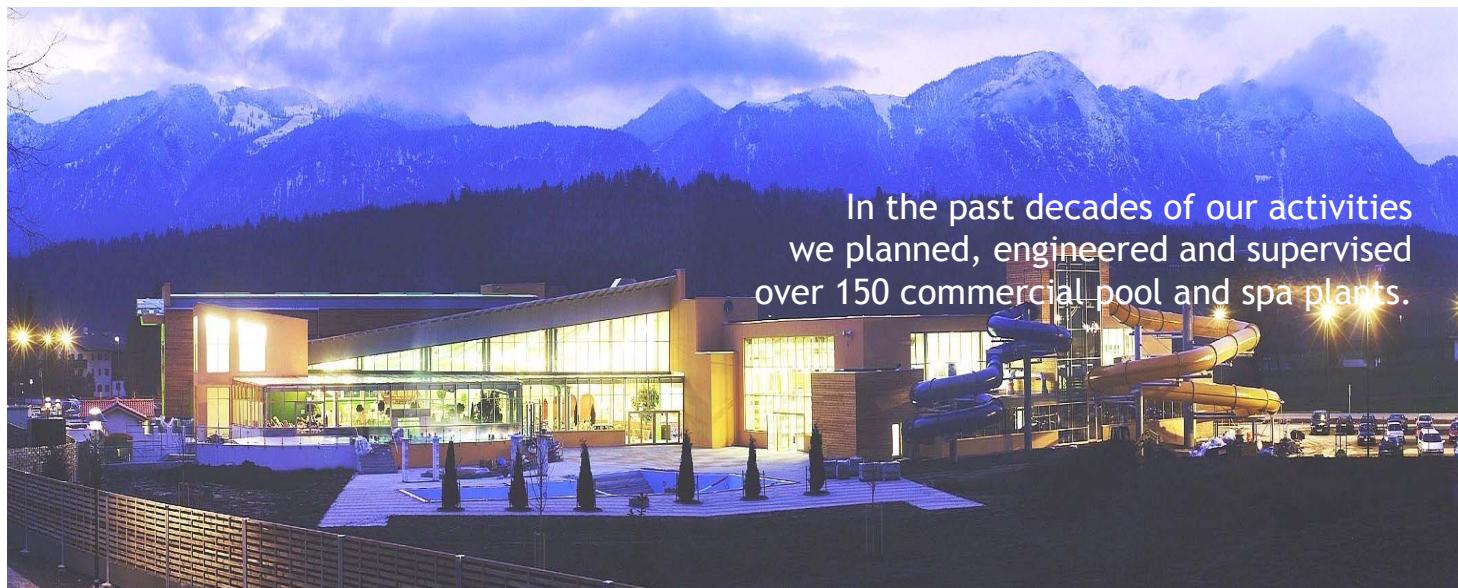
PfeifferPartner is known as the independent and objective specialists and experts in planning Hot Spring Spas, Water Parks and commercial recreation and wellness



PfeifferPartner works within EC and internationally in project development, planning, realization and operation of all ranges and types of water leisure plants.

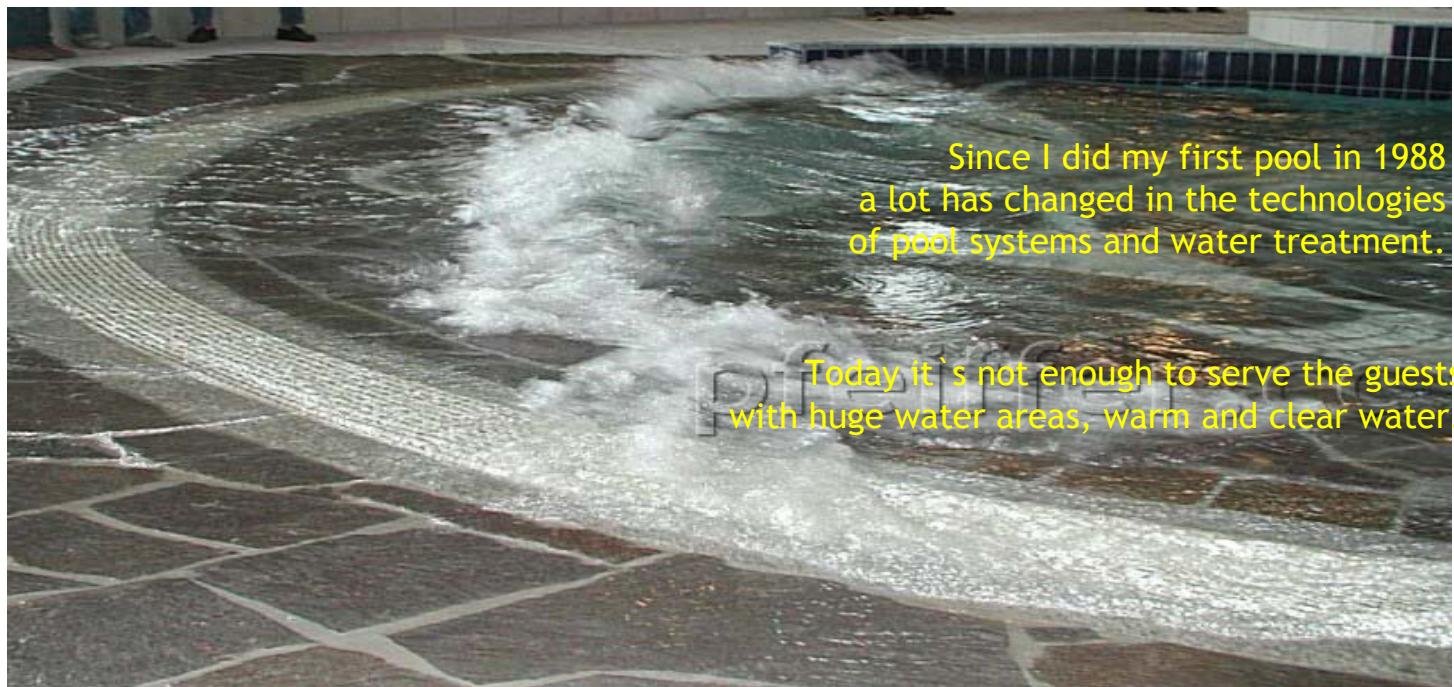
From Green Field Projects of Hot Spring Spas, full-year-spas or summer-spas to the revitalization of public or hotel spa's.





In the past decades of our activities we planned, engineered and supervised over 150 commercial pool and spa plants.





Since I did my first pool in 1988
a lot has changed in the technologies
of pool systems and water treatment.

Today it's not enough to serve the guests
with huge water areas, warm and clear water.

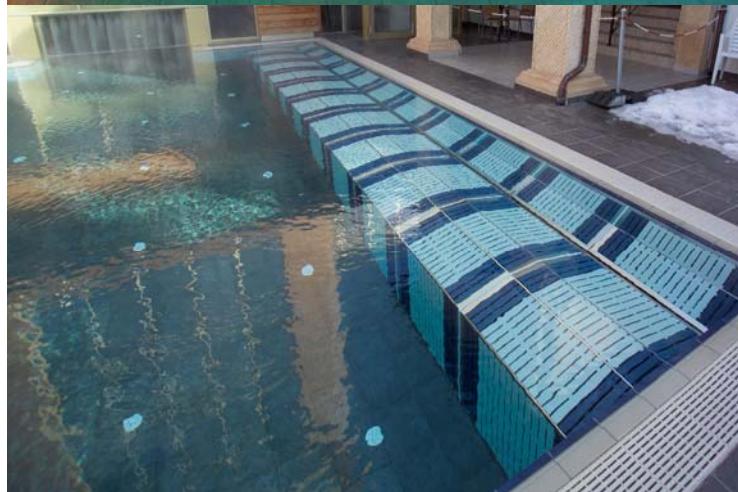


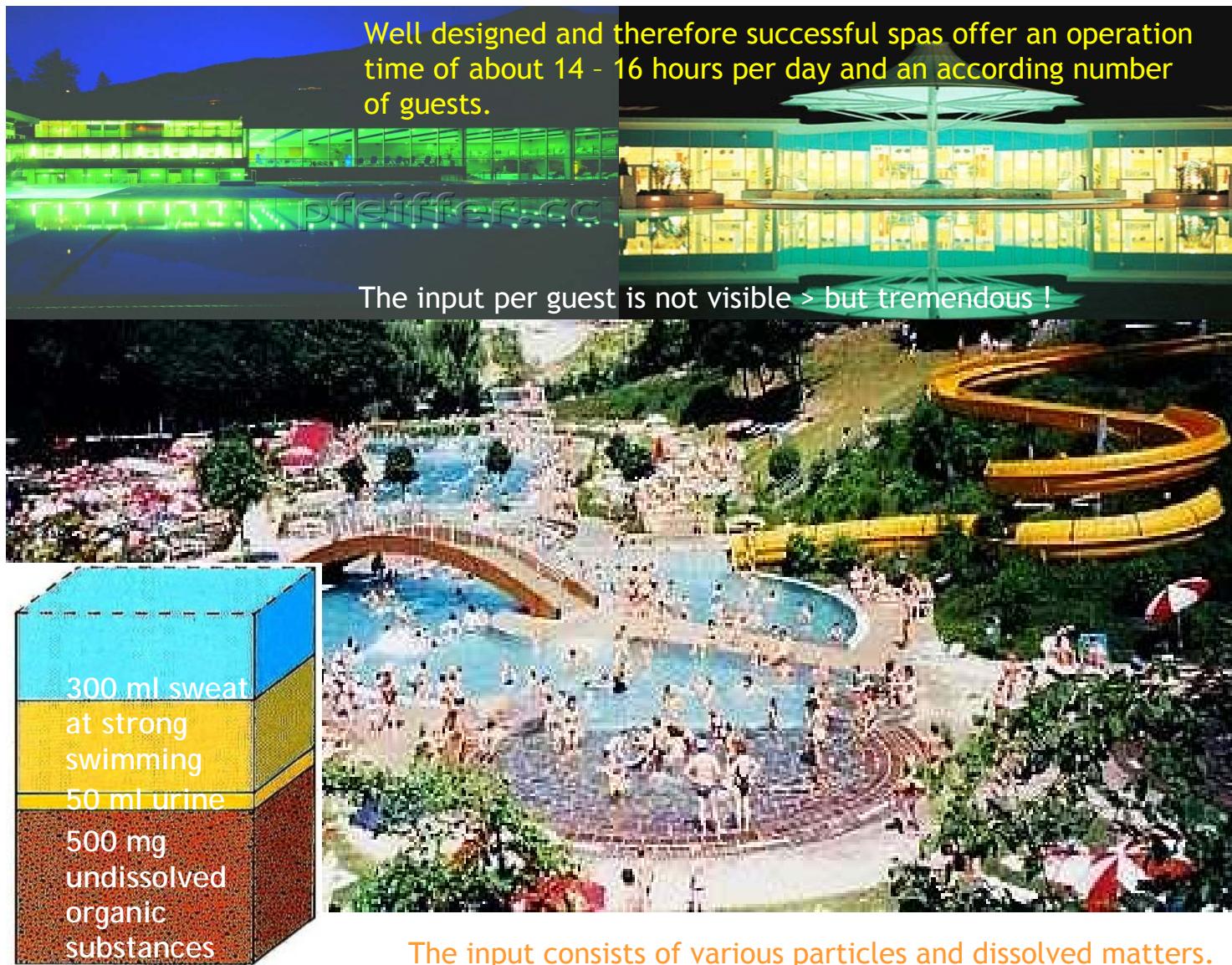
We designed attractions as
the beach with rolling waves,
and the „[wave behind glass](#)“, that
have been approved and often repeated.



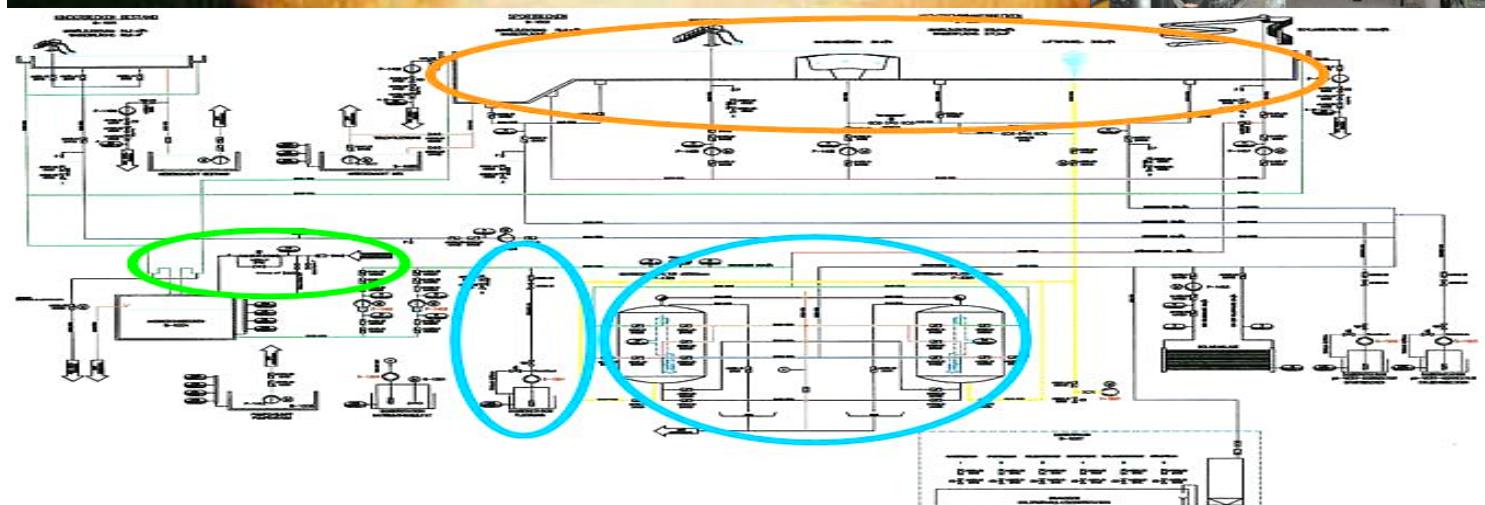
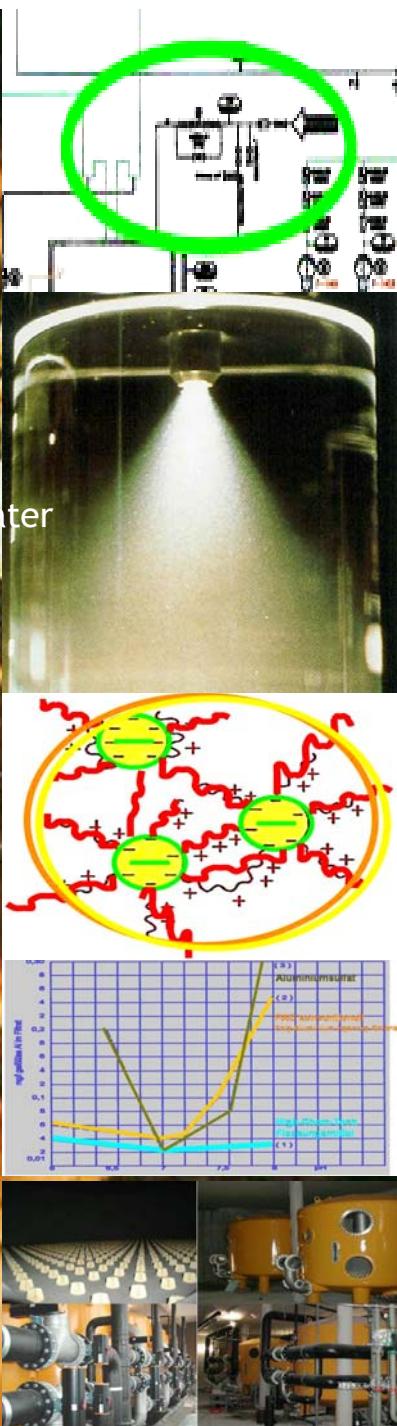
A successful example
is the construction and engineering
of the „champagne bed“ that provides
the jacuzzi effect over the whole surface

The „champagne bed“ and the additional technics
can be mounted especially subsequent
to increase the attractivity in existing pools.



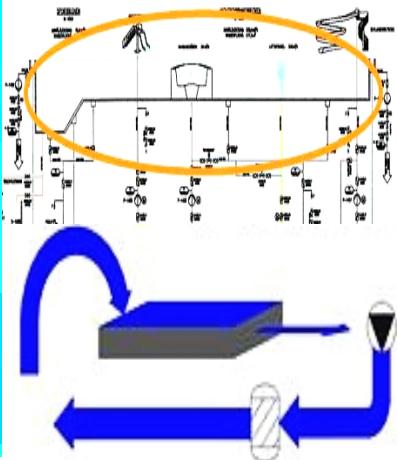


Mechanical Particles Sand, Dust, Hair, Dandruffs, Plant Particles	fine - middle granular 100 µm [0,1mm] - 5 mm	Hair + Fibre Prefilters Sedimentation, Filtration
Undissolved Suspended Dust, Spores, Pollen, Skin particles, Plant Particles	Coarse dispersed „molecular lumps“ 0,5 µm [0,0005mm] - 100 µm	Filtration with or without Flocculation Sand, Hydrocarbon,...
Colloides Spits, Slime, Fats, Oils, humine acids, precipitates..	Fine Dispersed „molecular lumps / threads“ 0,01 µm [0,00001mm] - 1µm	Flocculation + Filtration Adsorption Siliceous earth / Diatomeen
Dissolved Matters urea, sweat, Chloride, Nitrate, Phosphate, Iron, Gases, ..	Ions, Molecules bis 0,01 µm [0,00001mm]	Diluting, Oxidation, Adsorption Activated Carbon



Only an optimum flow system can maintain the renewal of pool water within shortest times and over the whole surface.

The right capacity has to be calculated according to several dimension parameters.



N = Persons /h

A = Pool Area [m²]

a = pool surface / person [1/m²]

k = treatment depending factor [1/m³]

$$N = \frac{A \times n}{a}$$

$$Q_{1-n} = \frac{N_{1-n}}{k} = \frac{A_{1-n} \times n}{a_{1-n} \times k} = [\text{m}^3/\text{h}]$$

Beckenart	Wassertiefe [m]	Wasserfläche je Person a [m ²]	Nennbelastung N [1/h]	Volumenstrom Q [m ³ /h]
Schwimmerbecken	>1,35	4,5	$\frac{0,222}{\text{m}^2 \times \text{h}} \times A$	$\frac{0,222}{\text{m}^2 \times \text{h}} \times \frac{A}{k}$
Nichtschwimmerbecken	0,6 – 1,35	2,7	$\frac{0,37}{\text{m}^2 \times \text{h}} \times A$	$\frac{0,37}{\text{m}^2 \times \text{h}} \times \frac{A}{k}$
Warmsprudelbecken (begrenzte Nutzung)	≤ 1,0	1 Sitzplatz	$\frac{3}{h} \times P$	$\frac{15}{h} \times V$
Warmsprudelbecken (kombinierte Nutzung) eigene Aufbereitung	≤ 1,0	—	$\frac{20}{h} \times k \times V$	$\frac{20}{h} \times V$
Warmsprudelbecken (kombinierte Nutzung) angeschlossene Aufbereitung	≤ 1,0	—	$\frac{10}{h} \times k \times V$	$\frac{10}{h} \times V$
Therapiebecken	≤ 1,35	4	$\frac{1}{h} \times k \times V$	$\frac{1}{h} \times A$

Example Kombi-Pool 25 x 10 m with 2 zones:

1. Non swimming [D<1,35M]
2. swimming [D>1,35M]

$$10 \times 10 \text{ m} = 100 \text{ m}^2$$

$$15 \times 10 \text{ m} = 150 \text{ m}^2$$

Capacity acc. to DIN 19643:

$$Q_1 = \frac{N_1}{k} = \frac{A_1 \times n}{a_1 \times k} = \frac{100 \times 1}{2,7 \times 0,5} = 74 \text{ m}^3/\text{h}$$

$$A_1 = 100 \text{ m}^2$$

$$n = 1/\text{h}$$

$$a_1 = 2,7 \text{ m}^2$$

$$k = 0,5 \text{ m}^{-3}$$

$$N_1 = \frac{A_1 \times n}{a_1} = \frac{100 \times 1}{2,7} = 37 \text{ h}^{-1}$$

$$Q_2 = \frac{N_2}{k} = \frac{A_2 \times n}{a_2 \times k} = \frac{150 \times 1}{4,5 \times 0,5} = 67 \text{ m}^3/\text{h}$$

$$A_2 = 150 \text{ m}^2$$

$$n = 1/\text{h}$$

$$a_2 = 4,5 \text{ m}^2$$

$$k = 0,5 \text{ m}^{-3}$$

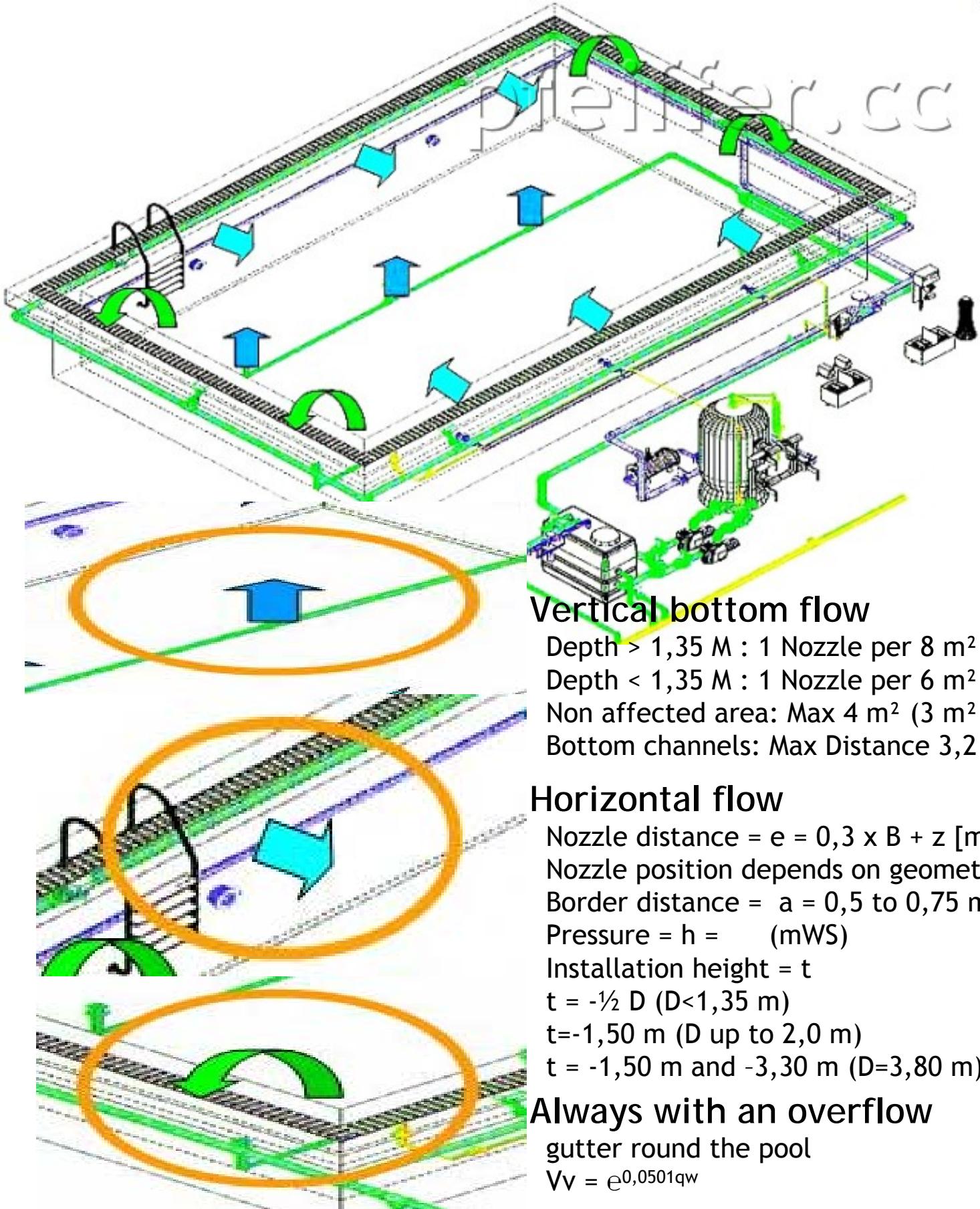
$$N_2 = \frac{A_2 \times n}{a_2} = \frac{150 \times 1}{4,5} = 33 \text{ h}^{-1}$$

Total capacity according to DIN 19643 is: $Q = Q_1 + Q_2 = 74 \text{ m}^3/\text{h} + 67 \text{ m}^3/\text{h} = 141 \text{ m}^3/\text{h}$

$$N = N_1 + N_2 = 37 \text{ h}^{-1} + 33 \text{ h}^{-1} = 70 \text{ h}^{-1} \text{ Persons per Hour}$$

E.g.: When the circulation is kept for 24 hours, 1.680 guests per day may use the pool..

Generally there are two possibilities
to maintain circulation through the pool



Vertical bottom flow

Depth > 1,35 M : 1 Nozzle per 8 m²
Depth < 1,35 M : 1 Nozzle per 6 m²
Non affected area: Max 4 m² (3 m²)
Bottom channels: Max Distance 3,2 m

Horizontal flow

Nozzle distance = $e = 0,3 \times B + z$ [m]
Nozzle position depends on geometry
Border distance = $a = 0,5$ to $0,75$ m
Pressure = $h =$ (mWS)
Installation height = t
 $t = -\frac{1}{2} D$ ($D < 1,35$ m)
 $t = -1,50$ m (D up to $2,0$ m)
 $t = -1,50$ m and $-3,30$ m ($D = 3,80$ m)

Always with an overflow

gutter round the pool

$$Vv = e^{0,0501qw}$$

\ Vertical bottom flow

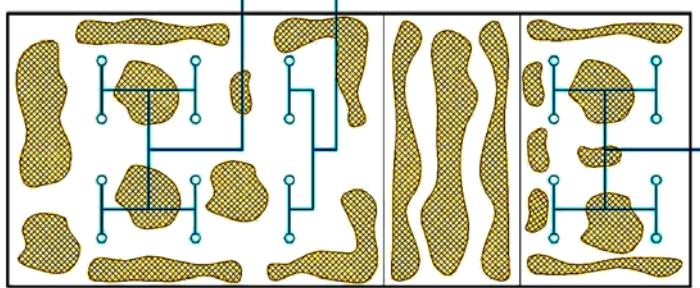
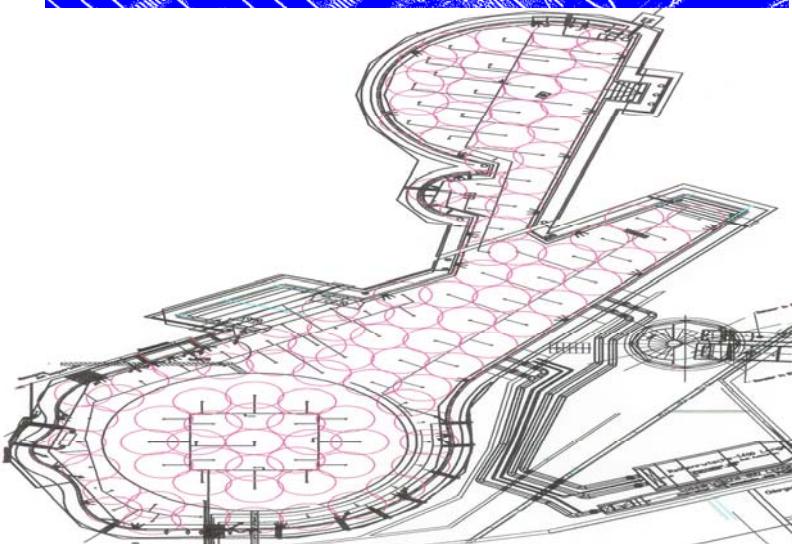
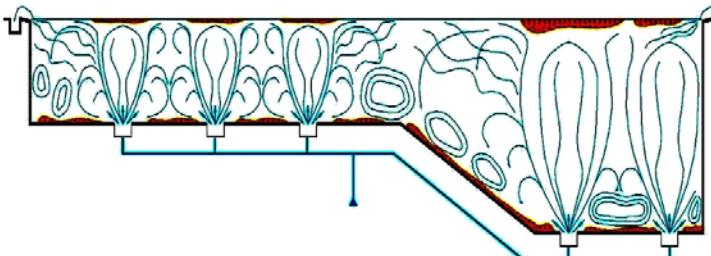
Vertical bottom flow is obtained by dividing the area through maximum possible flow rates

Depth > 1,35 M : 1 Nozzle per 8 m²

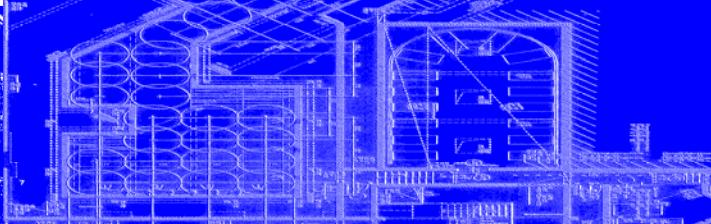
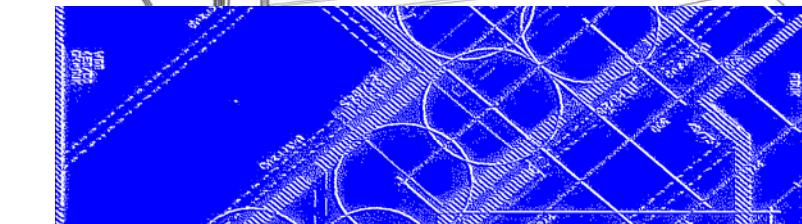
Depth < 1,35 M : 1 Nozzle per 6 m²

Non affected area: Max 4 m² (3 m²)

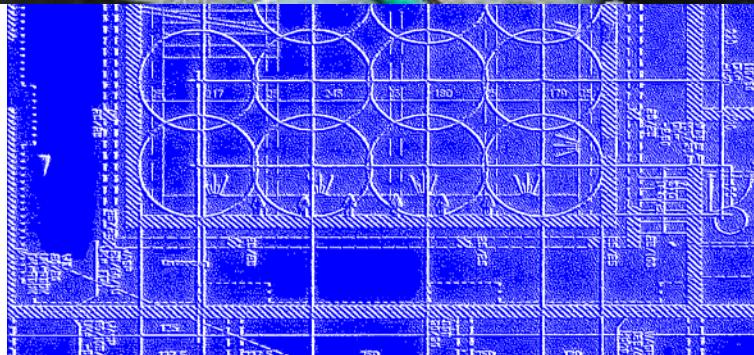
Bottom channels: Max Distance 3,2 m



This means a lot of dimensioning works for collecting, sub-collecting, sub-sub-collecting a.s.o. - pipes.



And the single-and-each nozzle-system means a tremendous afford in piping within the concrete bottom layer



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\ Vertical bottom flow

Engineering and prefabrication of bottom pipings may be handled by your experienced and skilled workers.

The real problems start when the realization of your works will meet to others on site.



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\ Bottom flow \ Effects

The dying test shows the results of all the engineering, piping works, coordinations, possible conflicts and mounting affordances

Laminar flow at bottom nozzles

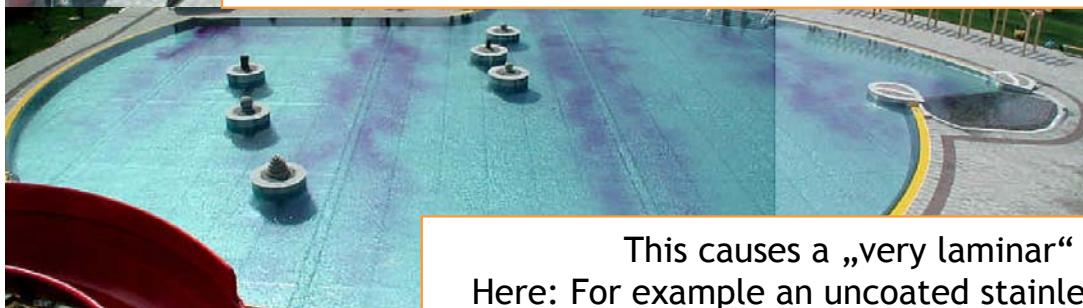
Following [not always..] the principle
„same amount per time and nozzle“

Another example

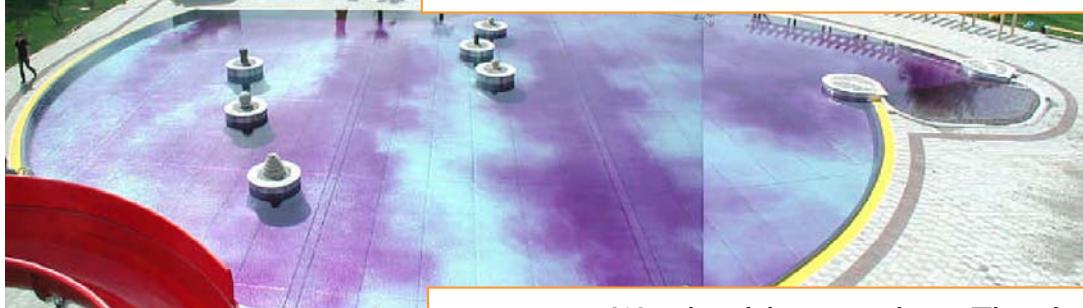
\ Bottom flow \ Effects



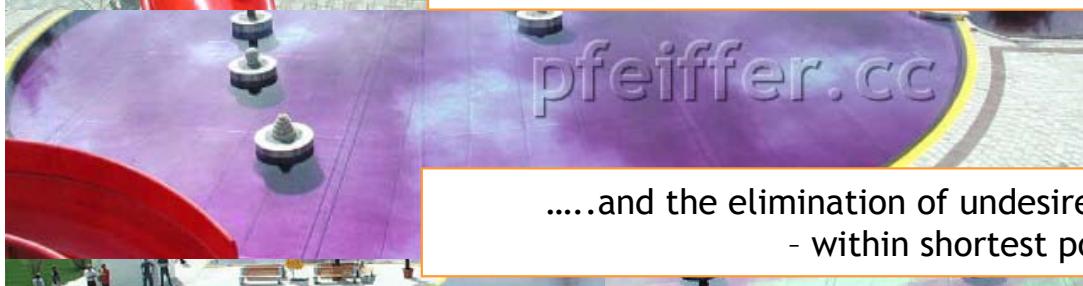
In contrast to bottom nozzles bottom channels are at least only „covered pipes“ with only one inlet and punched inlet openings.



This causes a „very laminar“ streaming in.
Here: For example an uncoated stainless steel pool.



We should remember: The dying test shows the distribution of disinfected treated water.....



.....and the elimination of undesired substances
- within shortest possible time..



Finally the deinking test shows the remaining weak zones (...that will remain for the next 30 years...)



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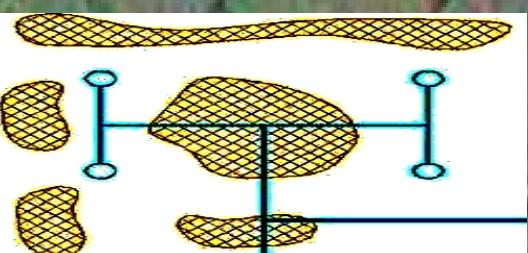
\ Summary \ bottom flow



- ❖ Traditionally accepted
„We did always so...for the past 40 y..“



- ❖ High material and work afford
- ❖ Renovation needs 2nd concrete layer
- ❖ Water treatment + Heating
only possible with filled pool



- ❖ No Up-Drifting of suspended particles
- ❖ Zones with high different chlorination,
algae growth, sediments and „dirt“
- ❖ No reduced capacity (night) possible

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\ What happened meanwhile..

While at the famous „Felsenthalerme“ in Bad Gastein one existing pool had been renovated with a **2nd concrete layer** and a **bottom flow system**, 50 meters away a new fun and recreation pool has been built up..

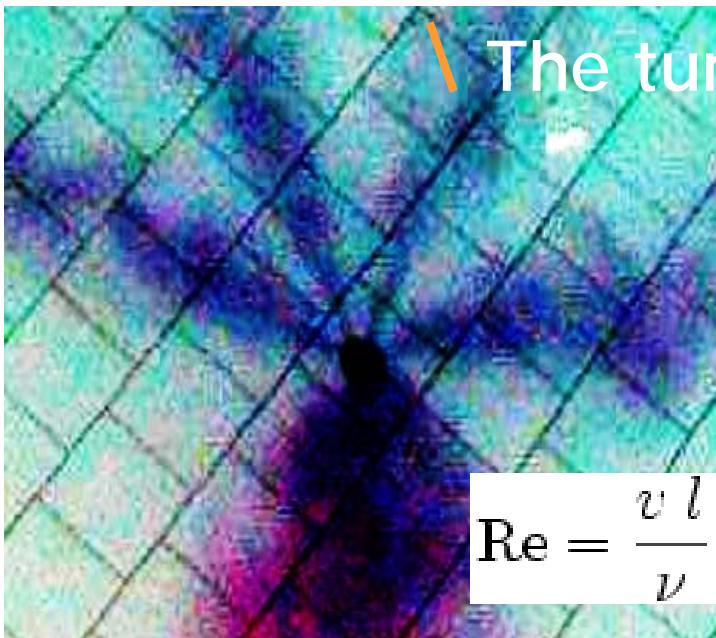


...with a Horizontal Flow
„Strahlenturbulenz“ system,
manufactured with 2 water levels.



There are no disturbing bottom inlets,
the pool has been built as a „stand-alone-solution“
within a defined concrete floor plate.

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\ The turbulence

was detected in 1883 by the physician Osborne Reynolds, when he recognized, that a fluid in a tube got over from laminar conditions, depending on velocity, length of the tube and a fluid depending parameter, the cinematic viscosity.

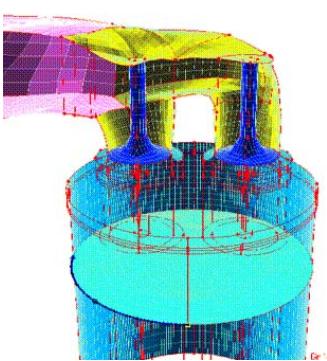
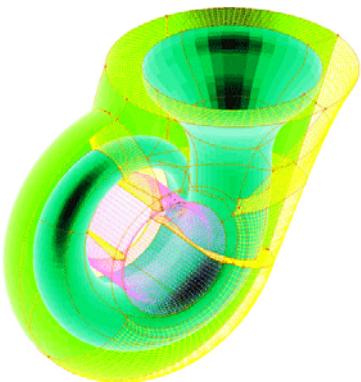
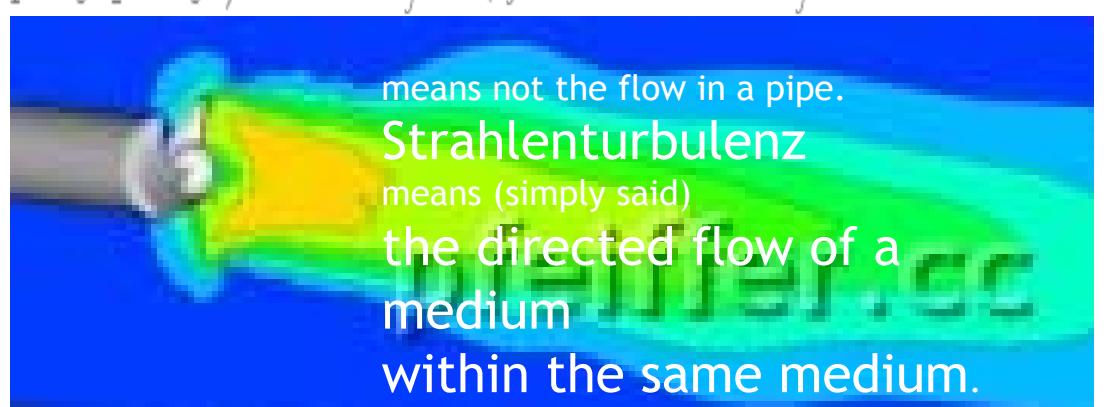
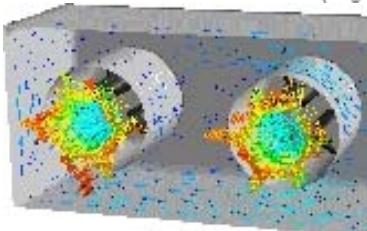
$$Re = \frac{v l}{\nu}$$

...I for myself enjoyed Reynolds, Nusselt, and his colleges during the 80's for his very interesting formulas in hydrodynamics...

$$\tau_{ij} = \rho \bar{u}'_i \bar{u}'_j = \rho \begin{pmatrix} \bar{u}_1'^2 & \bar{u}_1' \bar{u}_2' \\ \bar{u}_2' \bar{u}_1' & \bar{u}_2'^2 \\ \bar{u}_3' \bar{u}_1' & \bar{u}_3' \bar{u}_2' \end{pmatrix} A_i(r) = \sum_j m_j \frac{A_j}{\rho_j} W(r_i - r_j, h), r = \sum_j m_j \frac{A_j}{\rho_j} \nabla W(r_i - r_j, h).$$

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$$\rho_i(r) = \sum_j m_j \frac{\rho_j}{\rho_i} W(r_i - r_j, h) = \sum_j m_j W(r_i - r_j, h),$$

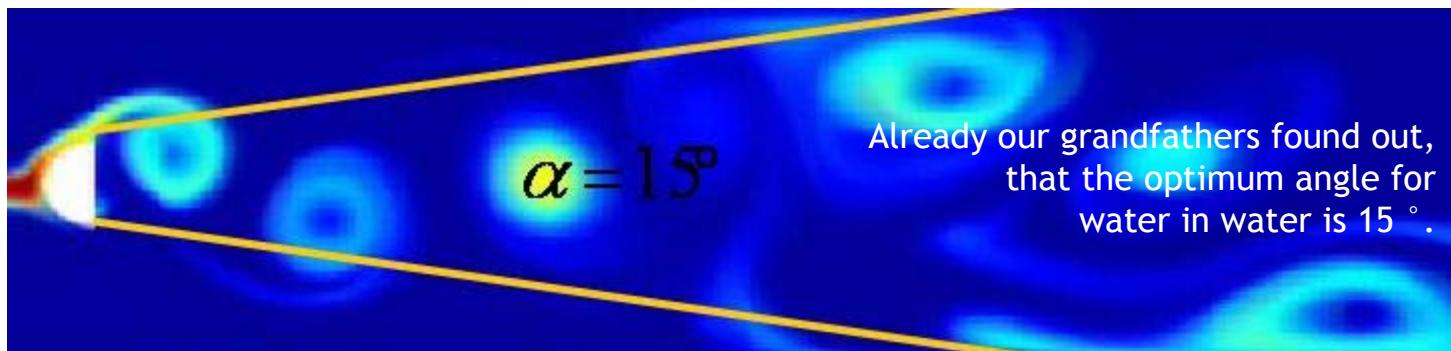
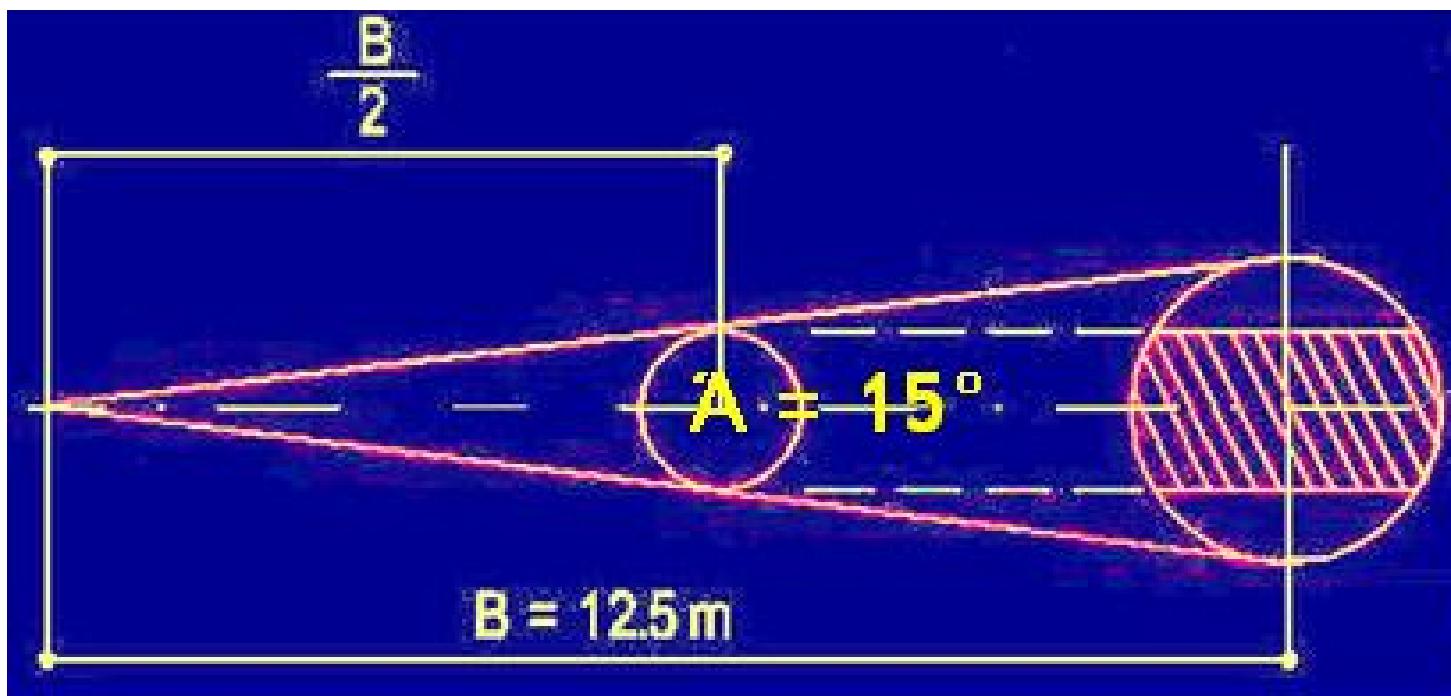


Strahlenturbulenz today is used e.g. in under water impellers, carburetors, common rail diesel engines or turbos.

Strahlenturbulenz has as well been used for about 500 Mio years in nature.

\ Directed flow
of a fluid within a fluid

\ Directed flow of a fluid within a fluid



Example

Reduced capacity (night)

$$Q_d = 20 \text{ m}^3/\text{h}$$

$$A_o \text{ at Staudruck} = 4 \text{ MWS} = 7,8 \text{ cm}^2$$

$$\text{Reduced } C = Q/2 = 10 \text{ m}^3/\text{h}$$

$$h_D = h/4 = 1 \text{ mWS} = v^2 = 35$$

$$V_m3 = 0,327 \text{ cm/s}$$

$$\text{Flow time} = 6,4 \text{ min at } Q = 10 \text{ m}^3/\text{h}$$

What does this mean in practice ?

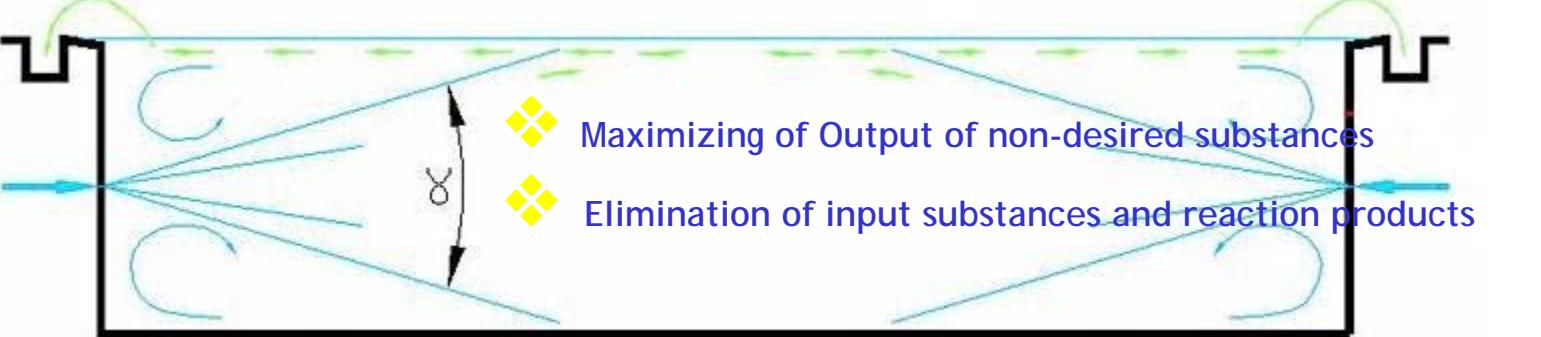
Let's have a look at the World Championship Competition Pool here in Montreal,

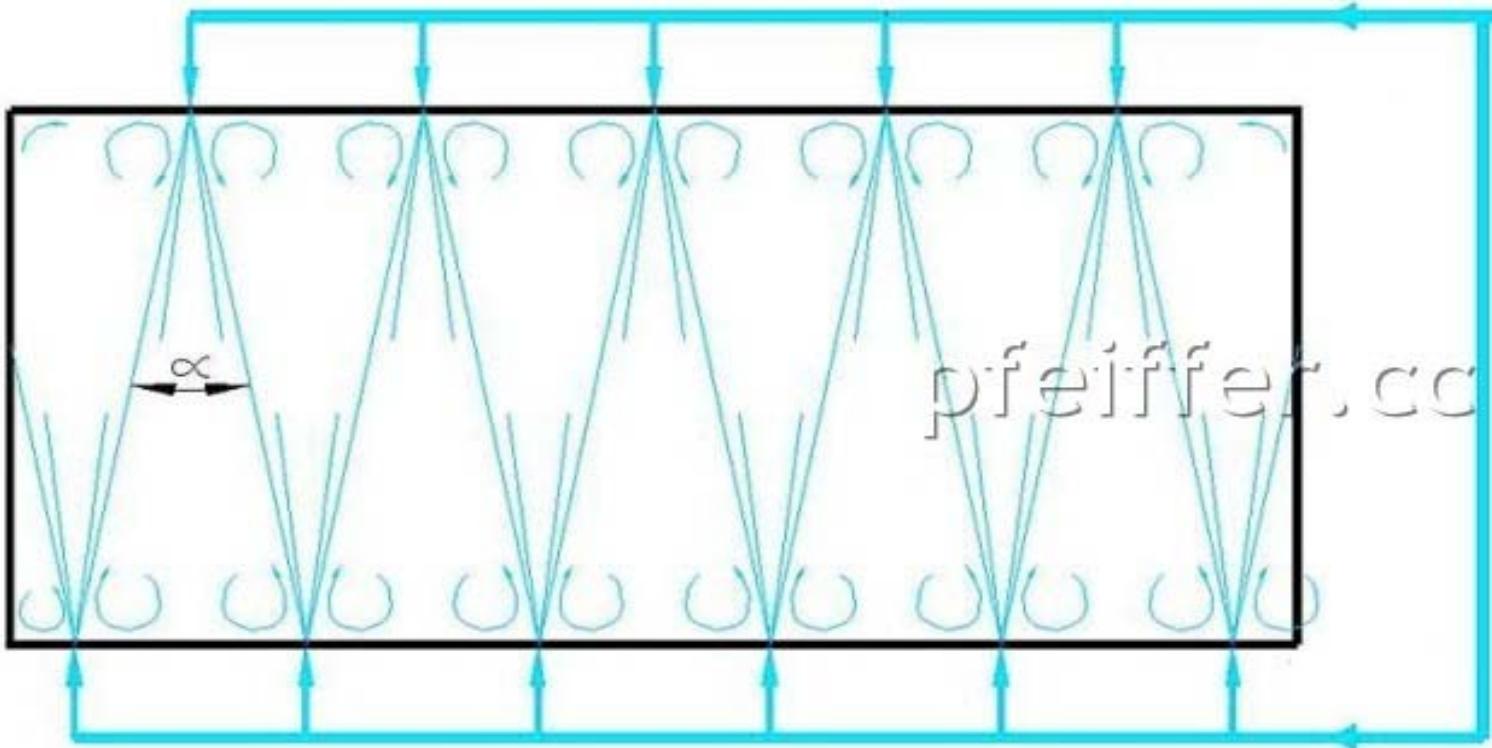
the pool construction and the flow system.

\ Calculations



Let us remember the possibilities in streaming in treated water and how to maintain a circulation that offers

- 
- ❖ Maximizing of Output of non-desired substances
 - ❖ Elimination of input substances and reaction products



Horizontal flow

Nozzle distance = $e = 0,3 \times B + z$ [m]

Nozzle position depends on geometry

Border distance = $a = 0,5$ to $0,75$ m

Pressure = $h =$ (mWS)

Installation height = t

$t = -\frac{1}{2} D$ ($D < 1,35$ m)

$t = -1,50$ m (D up to $2,0$ m)

$t = -1,50$ m and $-3,30$ m ($D = 3,80$ m)

\ Calculations

Datum:		Bearbeiter:		Tabelle A
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Beckenart:	Plan-Nr.:	Blatt:.....
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Pumpenleistung:.....m³/h;l/s		
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Förderhöhe:.....mWS		
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Beckenbreite:.....m		
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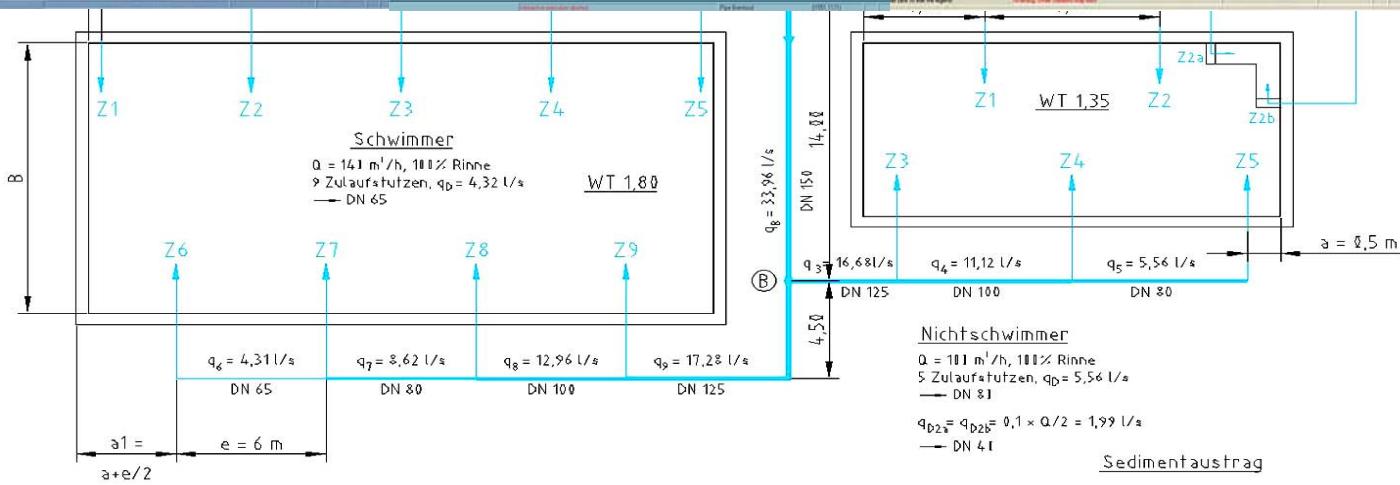
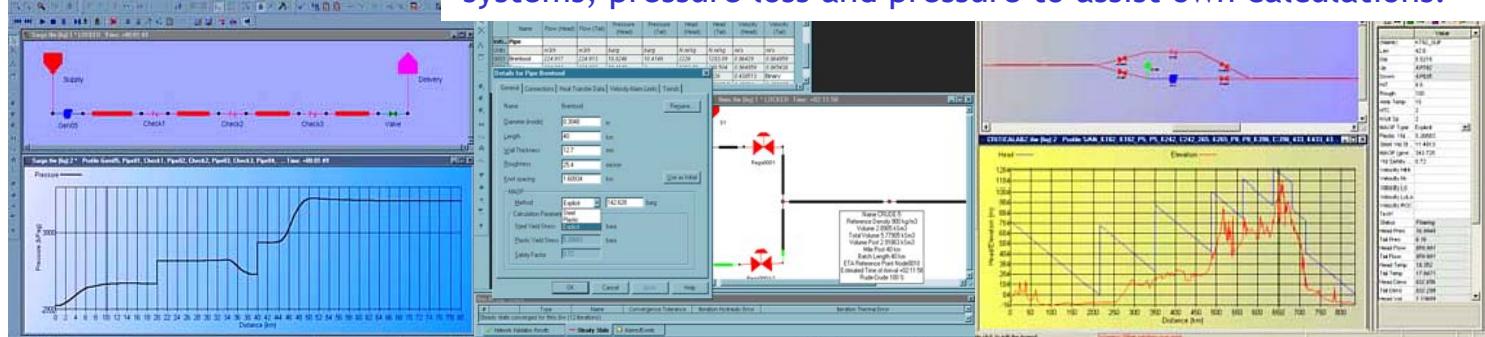
Staudruck:.....m	Düse:.....	Düsenart:.....
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Knoten	1	2	3	4	5	6	7	8=6 x 7	9	10	11	12	13	14	15
Richtung	Düse	Düse	q _D	Länge	Druckverlust	Druckverlust in der Zuleitung	h _D	Zuleitung	q _R	v = 3,56 · √h _D	A = q _D [l/s] / v [dm/s]	d = √(4 · A [dm²] / π)	d gewählt		
			DN	[l/s]	[m]	[mWS/m]	[mWS]	DN	[l/s]	[m/s]	[dm²]	[dm]	[mm]		
		Z6	65	4,32						6,70	0,064	0,2866	29,0		
1	Z7	65	4,32	6	0,042	0,252	3,792	65	4,32	6,93	0,062	0,2817	28,0		
1	Z8	65	4,32	6	0,050	0,300	4,092	80	8,64	7,20	0,060	0,2764	28,0		
1	Z9	65	4,32	6	0,037	0,222	4,314	100	12,96	7,39	0,058	0,2727	27,0		
B	1				6	0,021	0,126	4,440	125	17,28					
-1	Z3/N	65	5,56	4	0,020	0,080	4,360	125	16,68	7,43	0,075	0,3086	31,0		
-1	Z4/N	65	5,56	6	0,028	0,168	4,192	100	11,12	7,29	0,076	0,3116	30,5		
-1	Z5/N	65	5,56	6	0,022	0,132	4,060	80	5,56	7,17	0,078	0,3141	30,5		
A	1				10	0,026	0,260	4,700	150	33,96					
-1	Z5	65	4,32	3	0,032	0,096	4,604	125	21,6	7,64	0,057	0,2683	31,0		
-1	Z4	65	4,32	6	0,020	0,120	4,192	100	17,20	7,54	0,057	0,2704	30,5		
-1	Z3	65	4,32	6											

Depending on the capacity and the pool design the inlet and pressure of each nozzle is calculated.

Düsenart:.....

The market offers several programs for calculation of piping systems, pressure loss and pressure to assist own calculations.



Düsen-Staudruck: $h_D = \sqrt{B} \text{ [mWS]}$

$v_{Düse} = 3,56 \cdot \sqrt{h_D} = 3,56 = \text{konst.}$

Düsen-Abstand: $e = 1,3 \cdot B + x; x = 1,25 - 1,75 \text{ m (Fliesenraster)}$

Düsen-Randabstand: $a = 1,5 \pm 1,1 \text{ m}$

Düsen-Volumenstrom: $Q_B \text{ m}^3/\text{h} / \text{l/s}$

$z \times 3,6$

$I_{V \max} \text{ Stutzen} = 5 \%$

Düsen-Einbauhöhe: $WT \leq 1,35; t = WT/2$

$WT = 1,81; t = 1,51$

$WT = 3,81; t_1 = 1,51; t_2 = 3,31$

Rechnungsgang Schwimmer

1.) Ungünstiger Stutzen Z6 (Längste Zuleitung)

2.) $h = \sqrt{B} = \sqrt{12,5} = 3,54 \text{ mWS, gewählt } = 3,6 \text{ m WS } = Z_6$

3.) Rechnungsgang gem. [Tab. A]

Staudruck; $h_E \geq 1,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

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$h_E = h_A - l \times i_v$

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$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

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$h_E = h_A - l \times i_v$

$= 0,6 \text{ mWS}$

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$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

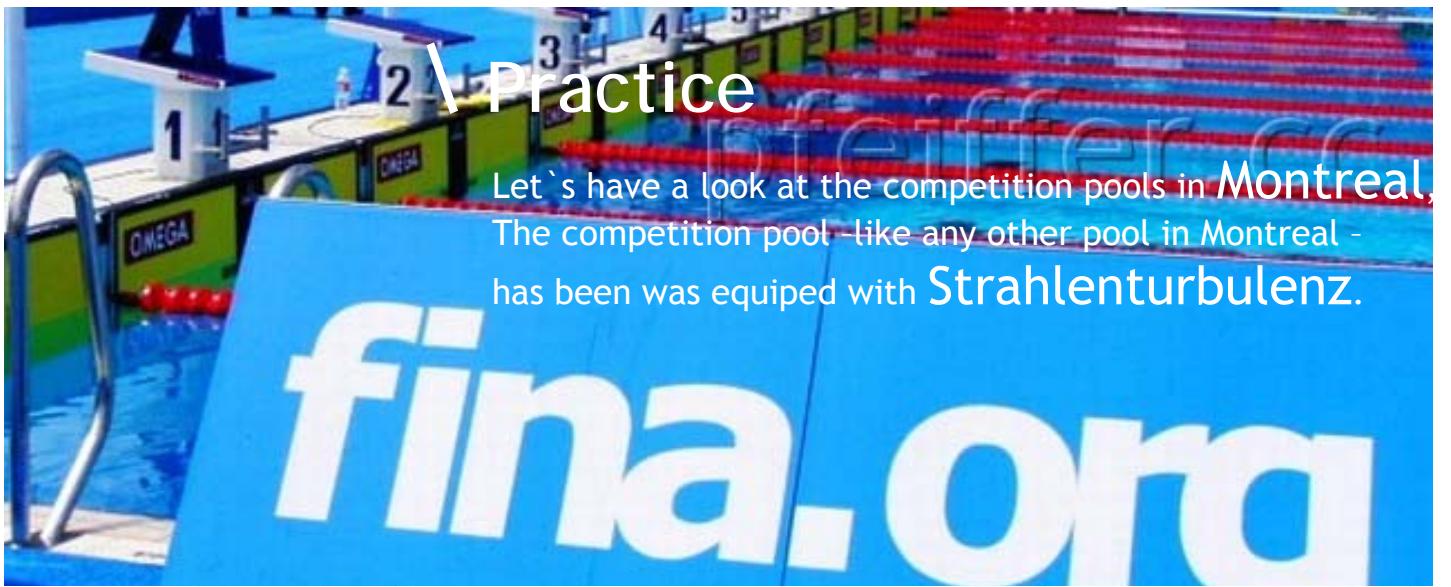
$= 0,6 \text{ mWS}$

$h_E = h_A + ex \times i_v$

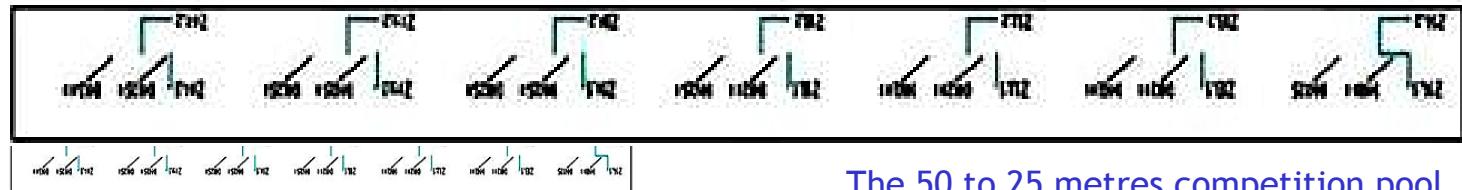
$= 0,6 \text{ mWS}$

$h_E = h_A - l \times i_v$

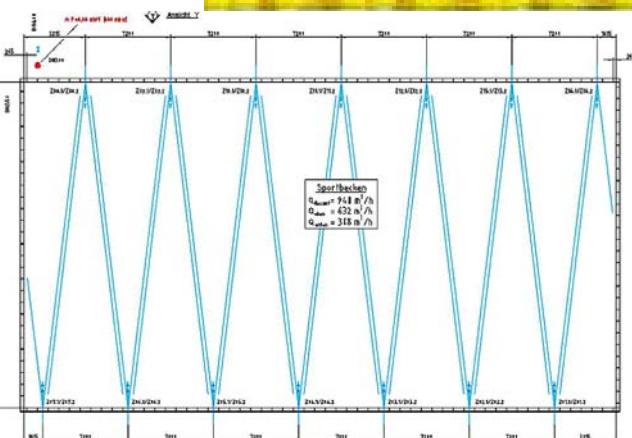
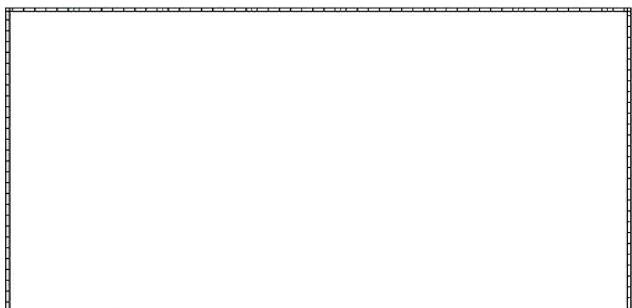
$= 0,6 \text{ mWS}$



Let's have a look at the competition pools in Montreal.
The competition pool -like any other pool in Montreal -
has been equipped with Strahlenturbulenz.



The 50 to 25 metres competition pool
has 7 pairs of Strahlenturbulenz nozzles
on each length side.

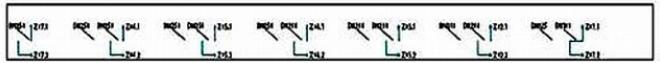
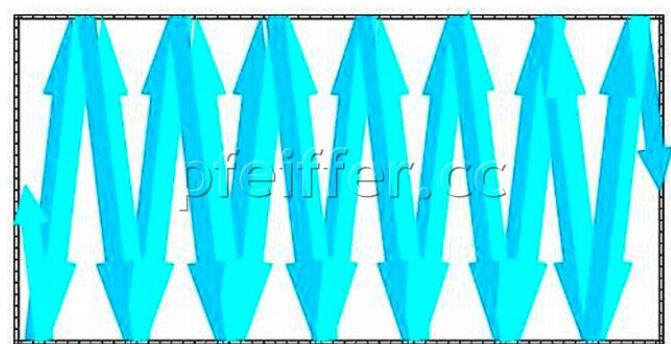
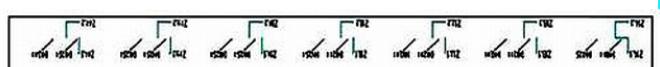
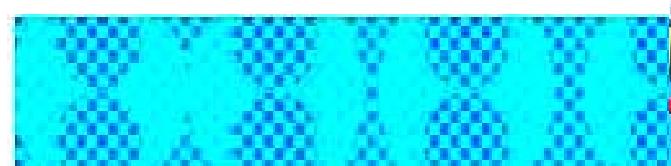
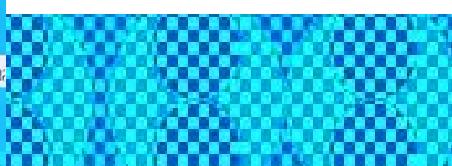
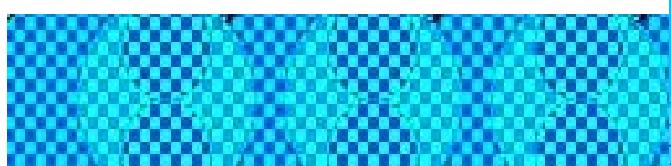
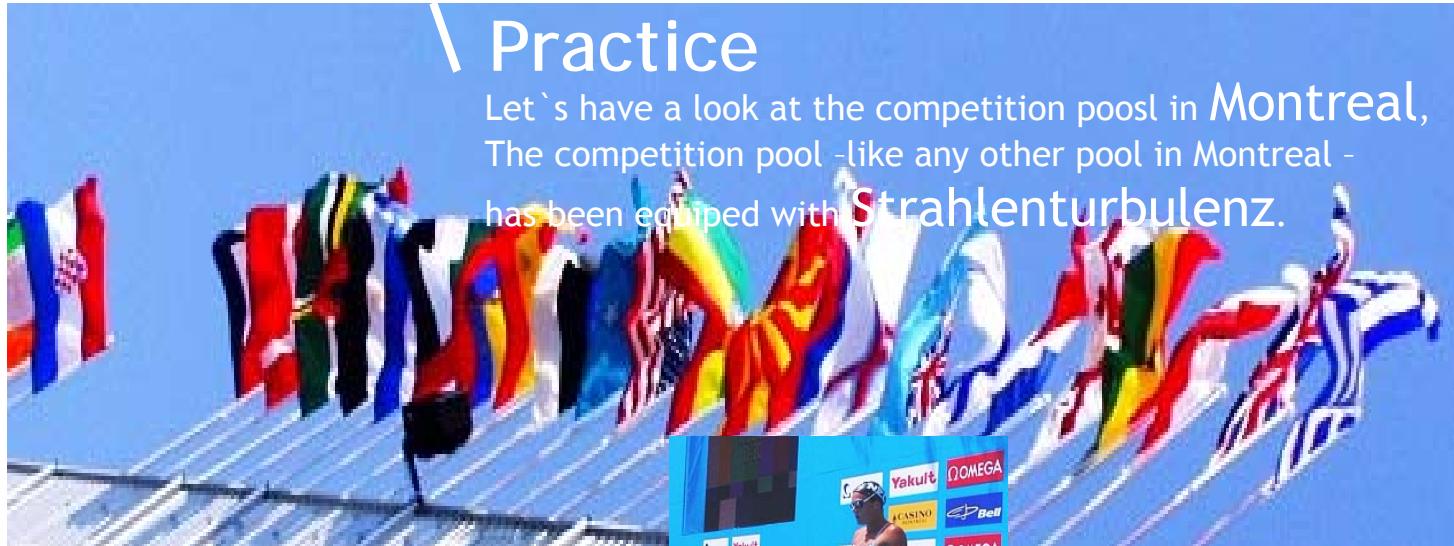


Each nozzle of each pair has been
dimensioned individually.

Depending on the individual
situation within the collecting
piping

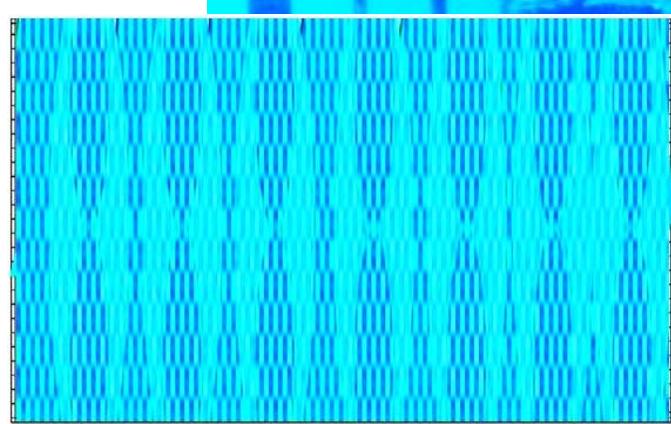
\ Practice

Let's have a look at the competition pool in Montreal,
The competition pool -like any other pool in Montreal -
has been equipped with Strahlenturbulenz.



The Strahlenturbulenz guarantees the distribution of treated water and elimination of input substances and reaction products within shortest time.

This is what the world's best swimmers have expecting at the FINA World Championship.



And what your customers and operators expect from your future pool projects !

\ Strahlenturbulenz
Summary



The Author
Karl Pfeiffer

has studied chemical technology [HTL], worked for several water treatment and pool engineering and design companies.

In 1988 he founded „Pfeiffer Engineering“ and expanded continuously in planning public pool plants, hot spas and water treatment plants.

In 2000 PfeifferPartner Ltd was established and partnerships have been growing internationally for projects within EC, the new neighbour states and overseas countries.

In 2005 Karl Pfeiffer was nominated by the courtyard as a permanent certified expert.

For additional questions **contact**

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We invite you,

to have a look at some of our [references](#) and some interesting and creative details in our [galery](#).